

We claim:

1. A process for removing N<sub>2</sub>O in nitric acid manufacture, which comprises utilizing catalysts comprising wire wovens and/or drawn-loop knits composed of high-temperature-stable materials and coated with catalytically active materials.
2. A process for removing N<sub>2</sub>O in nitric acid manufacture, wherein the wire wovens and/or drawn-loop knits coated with catalytically active materials consist of Fe-Cr-Al alloys.
3. The process for removing N<sub>2</sub>O in nitric acid manufacture according to claim 1 or 2 wherein the wire or the wire wovens and/or drawn-loop knits composed of high-temperature-stable materials are heat treated at from 100 to 1500°C prior to coating.
4. The process for removing N<sub>2</sub>O in nitric acid manufacture according to any of claims 1, 2 or 3 wherein the wire woven and/or drawn-loop knit coated with catalytically active materials forms a catalyst bed from 1 to 150 cm deep.
5. The process for removing N<sub>2</sub>O in nitric acid manufacture according to any of claims 1, 2, 3 or 4 wherein the temperature at the wire woven and/or drawn-loop knit coated with catalytically active materials is in the range from 500 to 980°C.
6. The process for removing N<sub>2</sub>O in nitric acid manufacture according to any of claims 1, 2, 3, 4 or 5 wherein the residence time over the wire woven and/or drawn-loop knit coated with catalytically active materials is less than 1 second.
7. A catalyst for removing N<sub>2</sub>O in nitric acid manufacture, constructed of a wire woven and/or drawn-loop knit composed of high-temperature-stable materials and coated with catalytically active materials.
8. A reactor for catalytic oxidation of ammonia to nitrogen oxides which comprises a noble metal catalyst, if appropriate a noble metal recovery network and a heat exchanger in the stated order in the flow direction, characterized in that a wire woven and/or drawn-loop knit composed of high-temperature-stable materials and coated with catalytically active materials is disposed between the noble metal catalyst/optional noble metal recovery gauze and the heat exchanger.

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9. Apparatus for producing nitric acid from ammonia, comprising in the stated order

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- a) a reactor according to claim 8,
- b) an absorption unit for absorbing nitrogen oxides in an aqueous medium,  
and if appropriate
- c) a reduction unit for selective catalytic reduction of nitrogen oxides.